

A Numerical Study of the Effect of Viscous Dissipation on the Heat and Mass Transfer of a Rotatory Nano Fluid

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Abstract: Viscosity dissipation is the non-reversible conversion of mechanical energy into thermal energy that occurs when a fluid performs work on neighbouring layers as a result of the impact of shear forces. Thus, the purpose of this research is to address the viscous dissipation effect on boundary layer flow of rotating incompressible Cu-Water nanofluid over an elongating surface. The model equations are transformed into a set of nonlinear ordinary differential (ODE) equations using a similarity transformation prior to getting computationally analysed using the Lobatto III A method using MATLAB. The influence of various parameters such as Eckert number, rotation porosity parameter etc on the flow properties has been analysed. The analysis discloses that with the amplification of the rotation parameter, Eckert number, nanoparticle volume fraction, and the porosity the temperature of the fluid experiences an improvement. Moreover, the velocity in the secondary direction decreases with an increase in the rotation parameter.

Keywords: Boundary layer, rotatory flow, viscous dissipation, porous medium, Lobatto III A method.

I. INTRODUCTION

Viscous dissipation refers to the irreversible conversion of mechanical energy into kinetic energy that occurs as a result of fluid particle interactions. It is of importance in numerous applications such as the substantial temperature increase is found in high-velocity polymer manufacturing flows including as extrusion or injection moulding. The thin boundary layer surrounding fast aircraft experiences aerodynamic heating, which boosts skin temperature [1]. Viscosity dissipation and spontaneous convection flow were initially studied by Gebhart [2]. He found that in natural convection flows with significant gravitational effects or a liquid with a large Prandtl number, internal produced energy cannot be ignored. Hussanan et al [3] defined viscous dissipation as “the work done by a fluid on neighbouring layers due to the impact of shear forces”. Nur Syamila Yusof et al.,[4] studied “the steady-state flow of a non-Newtonian fluid (Casson fluid) across an exponentially porous, slippery Riga plate with thermal radiation and magnetic field effects”. They discovered that increasing the thermal and velocity slip parameters reduces the temperature. Using the Lobatto III A approach, Mohamad Shoaib et al [5] explored “heat and mass transfer in 3D radiative flow of hybrid nanofluid across a rotating disc”. They discovered that temperature distribution is related to Brinkman number [5].

Heat transfer is crucial in many fields including biomedical, material science, oceanographic, nanotechnology, inorganic chemistry, and many more [6]. It is used in several technical advancements such as liquid distillation, heat exchange, and atomic controller refrigeration. In fluid mechanics, viscosity causes resistance to fluid motion, converting mechanical energy into heat energy. Thus, it is termed as internal energy shift [7]. Irfan Anjum Badruddin et al used the Finite element approach to explore the influence of viscous dissipation and heat radiation on natural convection in a porous material enclosed inside a vertical annulus tube and found that the average Nusselt number rises near the cold plate owing to increasing Ec values [8].

Nanofluid (NF) is a mixture of base fluid (water, ethanol etc) and nanoparticles. It is well known that the presence of nanomaterials alters the transporting characteristics and heat transfer efficiency in NF. The heat transmission qualities of a nanofluid are based on the mass fraction and thermophysical parameters of nanoparticles as well as the base fluid. These fluids are included in applications such as, oil exploration, metal extrusion, fiberglass polymer processing, continuous casting, plastic foil elongating and geothermal energy extraction. The thermal capacity of a NF with a permeable medium may be increased. Using nanoparticles in base liquids like oil, water, and ethylene glycol is a great way to improve heat transfer rate [9]. Research conducted on heat transfer intensification via NF can be identified in the series of the work.

In multiple procedures: such as temperature distribution, geothermal, enzymatic, nuclear reactor designs and earth sciences, there is the incorporation of convective flow in view of a porous media [10]. Permeable porous space is quite strong in subterranean systems, energy accumulating units, the circulation of water in supplies, photovoltaic reception, and so on. A large number of rotational “flows near stretchable or inextensible limits” are now being studied by academics. Zaimi et al. [11] constructed self-similar solutions for rotating viscoelastic fluid flow through an impermeable stretchable surface. Bakar et al [12] analysed “forced convection stagnation-point flow in a Darcy-Forchheimer porous medium towards a shrinking sheet”. Ullah et al. [13] investigated the “effect of velocity slip on MHD Casson fluid in a porous medium with nonlinear stretching”. Many researchers have engaged themselves in analysing the flow properties under various conditions in the presence of porous

medium due to its immense industrial and geophysical applications [14]–[18]. Due to its numerous useful applications in a wide range of engineering systems, boundary layer flows with internal heat generation over stretching sheets continue to be studied [1]. To best of the knowledge of the author the impact of internal energy on the rotary $Cu + H_2O$ flow in the presence of porous medium was not addressed by the researchers. Thus, the relevance of viscous dissipation to the thermal performance across a spinning sheet is underlined in this research.

II. MODELLING OF THE FLOW

Considering a steady, laminar, incompressible $Cu + water$ NF rotating flows over an expanding sheet in the presence of internal energy as shown in Figure 1. The fluid is assumed to flow in the $z > 0$ plane with the sheet elongating with a constant flow speed of $U_0 = bx$, where $b > 0$ is invariant. The velocity components in the cartesian plane are assumed to be u, v, w in the x, y & z - direction. The angular velocity of the flow is treated as Ψ . Further the flow is consistent with both ambient \ wall temperature and concentration.

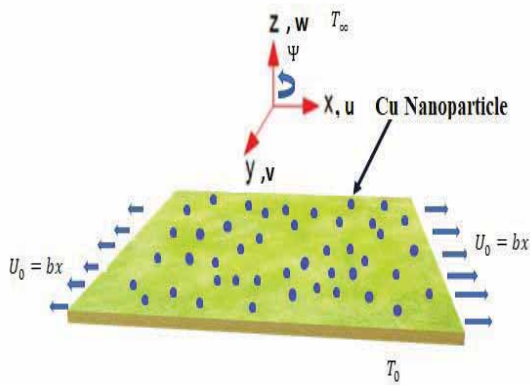


Figure 1. The physical model of the problem

“The Maxwell-Garnetts and Brinkman models are used to measure nano liquid thermal conductivity and dynamic viscosity”. These models characterize spherical nanoparticles with a volume fraction of $< 10\%$. Using the given hypotheses the boundary-layer flow governing equations are [19]

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad (1)$$

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = \frac{\mu_{nf}}{\rho_{nf}} \frac{\partial^2 u}{\partial z^2} + 2\Psi v - \frac{v_{nf}}{k_p} u \quad (2)$$

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = \frac{\mu_{nf}}{\rho_{nf}} \frac{\partial^2 v}{\partial z^2} - 2\Psi u - \frac{v_{nf}}{k_p} v \quad (3)$$

$$u \frac{\partial T}{\partial x} + v \frac{\partial T}{\partial y} + w \frac{\partial T}{\partial z} = \frac{k_{nf}}{(\rho C_p)_{nf}} \frac{\partial^2 T}{\partial z^2} + \frac{\mu_{nf}}{(\rho C_p)_{nf}} \left[\left(\frac{\partial u}{\partial z} \right)^2 + \left(\frac{\partial v}{\partial z} \right)^2 \right] \quad (4)$$

$$u \frac{\partial C}{\partial x} + v \frac{\partial C}{\partial y} + w \frac{\partial C}{\partial z} = D_{nf} \frac{\partial^2 C}{\partial z^2} \quad (5)$$

The end constraints are,

$$\begin{aligned} u &= U_0 ; v = 0 ; w = 0 ; T = T_0 ; \\ C &= C_0 \text{ at } z = 0 \\ u &\rightarrow 0 ; v \rightarrow 0 ; w \rightarrow 0 ; T \rightarrow T_\infty ; C \rightarrow C_\infty \\ &\text{as } z \rightarrow \infty \end{aligned} \quad (6)$$

μ_{nf} the dynamic viscosity [20], ρ_{nf} the density [21], k_{nf} the thermal conductivity [22], $(\rho C_p)_{nf}$ the heat capacitance [23], D_{nf} is the mass diffusivity [24] of the NF which are given by

$$\mu_{nf} = \frac{\mu_f}{(1 - \phi)^2}, \quad \rho_{nf} = (1 - \phi)\rho_f + \phi\rho_s \quad (7)$$

$$k_{nf} = k_f \left[\frac{k_s + 2k_f - 2\phi(k_f - k_s)}{k_s + 2k_f + \phi(k_f - k_s)} \right] \quad (8)$$

$$(\rho C_p)_{nf} = (1 - \phi)(\rho C_p)_f + \phi(\rho C_p)_s \quad (9)$$

$$D_{nf} = \frac{D_f}{1 - \phi} \quad (10)$$

The subscripts in the above equations indicate the properties of the NF, base fluid (water), solid Cu nanoparticle. The thermophysical properties required for the flow analysis are given below,

TABLE I.
PROPERTIES OF WATER AND SOLID COPPER NANO PARTICLE [25]

Properties	Base Fluid (Water)	Nano Particles (Cu)
Thermal Conductivity $(k) (Wm^{-1}K^{-1})$	0.613	400
Density $(\rho) (kgm^{-3})$	997.1	8933
Specific heat $(Cp) (Jkg^{-1}K^{-1})$	4179	385
$\beta (1/K)$	36.2×10^{-5}	1.67×10^{-5}

III. MATHEMATICAL TECHNIQUE

Let us consider the following similarity transformations [19], [22], [26]

$$\left. \begin{aligned} \eta &= \sqrt{\frac{a}{v}}z, u = axF'(\eta), v = axG(\eta), \\ w &= -\sqrt{av}F(\eta), \theta(\eta) = \frac{T-T_\infty}{T_0-T_\infty}, \\ \Phi(\eta) &= \frac{c-c_\infty}{c_0-c_\infty} \end{aligned} \right\} \quad (11)$$

Substituting these into the equations to, equation (1) is satisfied and the remaining equations (2)-(5), along with the boundary conditions(6), transform into highly non-linear ODE, which can be given as

$$\frac{\mu_{nf} \rho_f}{\mu_f \rho_{nf}} F''' = (F')^2 - FF'' - 2R_0G + k_1F' \quad (12)$$

$$\frac{\mu_{nf} \rho_f}{\mu_f \rho_{nf}} G'' = F'G - G'F + 2R_0F' + k_1G \quad (13)$$

$$\frac{k_{nf} (\rho C_p)_f}{k_f (\rho C_p)_{nf}} [\theta''] = -(Pr (F\theta' \quad (14)$$

$$+ Ec((F'')^2 + (G')^2)) \quad (15)$$

$$\Phi'' + \frac{Sc}{(1-\phi)} F\Phi' = 0$$

With the BCs,

$$\left. \begin{aligned} F'(\eta) &= 1, G(\eta) = 0, F(\eta) = 0, \\ \theta(\eta) &= 1, \Phi(\eta) = 1 \text{ at } \eta = 0 \\ F'(\eta) &\rightarrow 0, G(\eta) \rightarrow 0, \\ \theta(\eta) &\rightarrow 0, \Phi(\eta) \rightarrow 0 \text{ as } \eta \rightarrow \infty \end{aligned} \right\} \quad (16)$$

The parameters involved in the above equations are [19],[27]

$$\text{Eckert number : } Ec = \frac{\rho_f U_0^2}{(\rho C_p)_f (T_\infty - T_0)},$$

$$\text{Porosity parameter: } k_1 = \frac{v_f}{bk_p}$$

$$\text{Rotational parameter: } R_0 = \frac{\psi}{b}$$

$$\text{Prandtl number : } Pr = \frac{v_f}{\alpha_f},$$

$$\text{Schmidt number : } Sc = \frac{v_f}{D_f}$$

The expression for the local drag force coefficients [19] C_{fx} and C_{fy} , heat transfer coefficient Nu_x and the mass transfer coefficient Sh_x can be defined as

$$C_{fx} \equiv \frac{\tau_{xz}}{\frac{1}{2}\rho U_0^2}, C_{fy} \equiv \frac{\tau_{yz}}{\frac{1}{2}\rho U_0^2},$$

$$Nu = \frac{xq_w}{k(T_0 - T_\infty)}, \text{ and}$$

$$Sh_x = \frac{xq_m}{D_M(C_0 - C_\infty)}$$

In which τ_{xz}, τ_{yz} signify the tensors of shear stress and q_w, q_m represent “the heat and mass flux at the sheet walls”. Applying the transformations, the above expressions transform into,

$$Re_x^{\frac{1}{2}} C_{fx} = \frac{\mu_{nf}}{\mu_f} F''(0)$$

$$Re_x^{1/2} C_{fy} = \frac{\mu_{nf}}{\mu_f} G'(0) \quad (17)$$

$$Re_x^{-1/2} Nu_x = -\frac{k_{nf}}{k_f} \theta'(0)$$

$$Re_x^{-1/2} Sh_x = -\frac{D_{nf}}{D_f} \Phi'(0)$$

IV. SOLUTION METHODOLOGY

The non-dimensional ODEs are set into a linear format using the relations,

$$\left. \begin{aligned} f_1 &= F, f_2 = F', f_3 = F'', F''' = f_3' \\ &= -A_1 A_2 [f_1 f_3 + 2R_0 g_1 \\ &\quad - (f_2)^2 + k_1 f_2] \end{aligned} \right\} \quad (18)$$

$$\left. \begin{aligned} g_1 &= G, g_2 = G', G'' = g_2' \\ &= A_1 A_2 [-f_1 g_2 + 2R_0 f_1 \\ &\quad + f_2 g_1 + k_1 g_1] \end{aligned} \right\} \quad (19)$$

$$\left. \begin{aligned} \theta_1 &= \theta(\eta), \theta_2 = \theta'(\eta), \theta_3 = \theta_2' \\ &= -\frac{Pr * k_f}{k_{nf}} [A_3 f_1 \theta_2 \\ &\quad + Ec[f_3^2 + g_2^2]] \end{aligned} \right\} \quad (20)$$

$$\Phi_1 = \Phi, \Phi_2 = \Phi', \Phi_3 = -\frac{Sc f \Phi'}{(1-\phi)} \quad (21)$$

$$\text{Here, } A_1 = \frac{\mu_f}{\mu_{nf}}, A_2 = \frac{\rho_{nf}}{\rho_f}, A_3 = \frac{[\rho C_p]_{nf}}{[\rho C_p]_f} \quad (22)$$

Along with the modified BCs

$$f_1 = 0, f_2 = 1, g_1 = 0, \theta_1 = 1, \Phi_1 = 1 \text{ as } \eta = 0$$

$$f_2 \rightarrow 0, g_1 \rightarrow 0, \theta_1 \rightarrow 0, \Phi_1 \rightarrow 0 \text{ as } \eta \rightarrow \infty$$

The set of equations (12)-(15), along with the prescribed conditions (16), has been solved using the bvp4c solver which performs the finite difference code that implements the three-stage Lobatto IIIA formula of fourth-order [28]. The system is solved with absolute and relative accuracy of order 10^{-6} .

The MATLAB BVP4C implements Lobatto IIIA collocation RK method [29]– [33]. The validation of the code was verified by comparing the results by determining the values of C_{fx}, C_{fy} and Nu_x for the base fluid and matched with the formerly available papers in TABLE 4 and TABLE 3

TABLE II.
COMPARISON OF THE VALUES OF $Re_x^{1/2} C_{fx}$ and $Re_x^{1/2} C_{fy}$ FOR BASE FLUID WHEN $\phi = Ri = A = B = Sc = 0$

	Nor Azizah Yacob et al[34]		N. A. Salleh, et al[35]		Present findings	
R_0	$-\frac{\mu_{nf}}{\mu_f} F''(0)$	$-\frac{\mu_{nf}}{\mu_f} G'(0)$	$-\frac{\mu_{nf}}{\mu_f} F''(0)$	$-\frac{\mu_{nf}}{\mu_f} G'(0)$	$-\frac{\mu_{nf}}{\mu_f} F''(0)$	$-\frac{\mu_{nf}}{\mu_f} G'(0)$
0.0	1.00000	0.00000	1.000000	0.000000	1.00000	0.000000
0.5	1.13838	0.51276	1.138381	0.512760	1.138411	0.512802
1.0	1.32503	0.83809	1.325029	0.837098	1.325031	0.837121
2.0	1.6524	1.28726	1.652352	1.287259	1.652392	1.287301

TABLE III.
COMPARISON OF CALCULATED VALUES OF $Re_x^{-0.5} Nu_x$ FOR BASE FLUID.

	Nadeem et al. [36]	N. A. Salleh, et al [35]	Current findings
R_0	$\frac{-k_{nf}}{k_f} \theta'(0)$	$\frac{-k_{nf}}{k_f} \theta'(0)$	$\frac{-k_{nf}}{k_f} \theta'(0)$
0.00	1.770948	1.770948	1.77094791
0.50	1.725631	1.725631	1.72563892
1.00	1.660286	1.660286	1.66028591
2.00	1.533487	1.533487	1.53348701

V. RESULTS AND DISCUSSION

To analyse the predominance of the parameters such as Eckert number, porosity etc involved in the governing ODEs of the rotary NF flow over a linearly stretching sheet in the presence of internal energy and porous medium the Lobatto IIIA collocation method has been utilised. The results obtained have been graphed, tabulated, and discussed below.

The values of parameters throughout the analysis have been considered as $Ec = 0.2, k_1 = 0.5, Sc = 0.5, R_0 = 0.2, \phi = 0.02$, except for the modifications required in the corresponding figures.

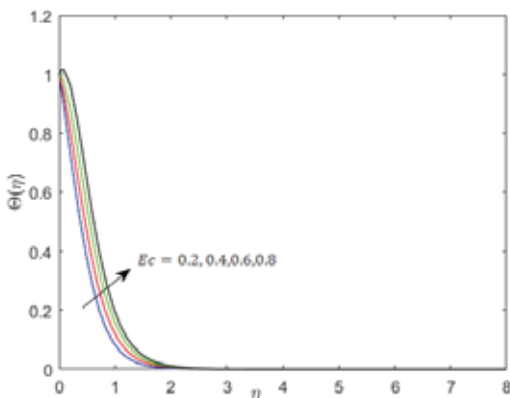


Figure 2. Effect of Eckert number on the Temperature profile

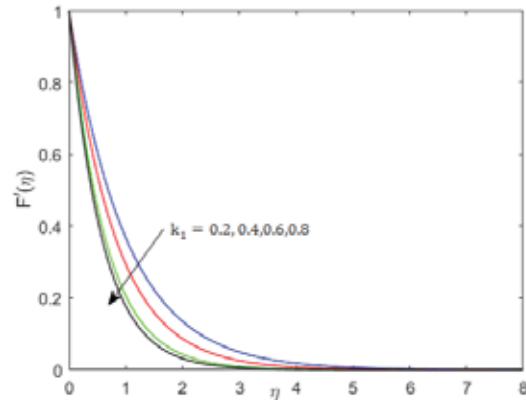


Figure 3. The Predominance of k_1 (porosity parameter) value on PVG

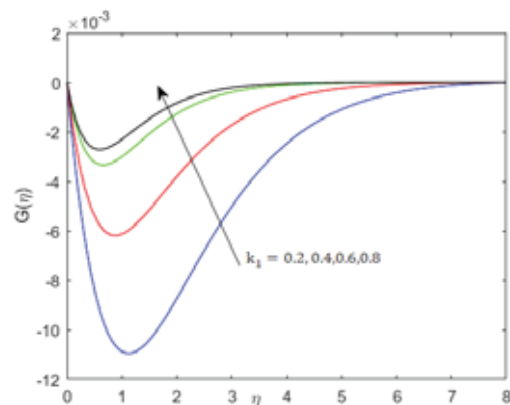


Figure 4. Impact of k_1 on the SVG

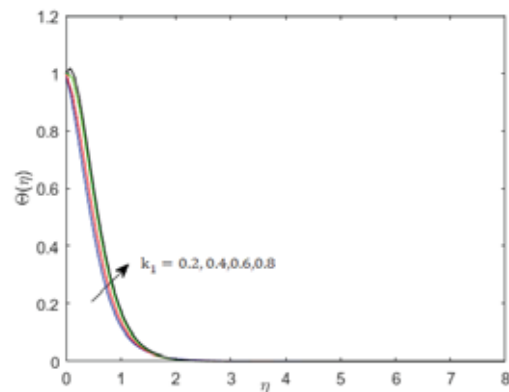


Figure 5. Effect of k_1 on $\theta(\eta)$

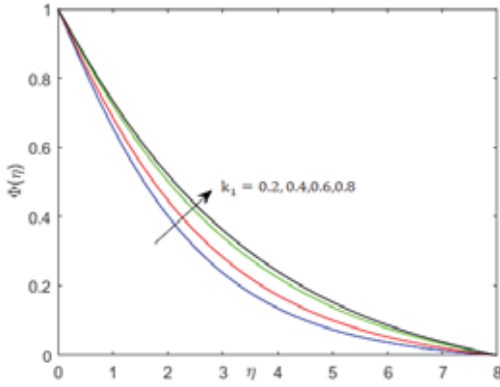


Figure 6. Effect of k_1 on $\Phi(\eta)$

Figure 3-Figure 6 demonstrates the porosity parameter's role on the physical properties of the NF flow. Higher porosity increases the impulse and speeds the flow, whereas it decelerates the flow for small pore size by increasing the “viscous drag of the porous channel” [37]. Thus, the improvement in values of k_1 leads to the enlargement of the temperature, SVG, and concentration profiles whereas the impact is opposite on PVG. And also, we observe that the increase in the porosity leads to the increase in both temperature and concentration profiles.

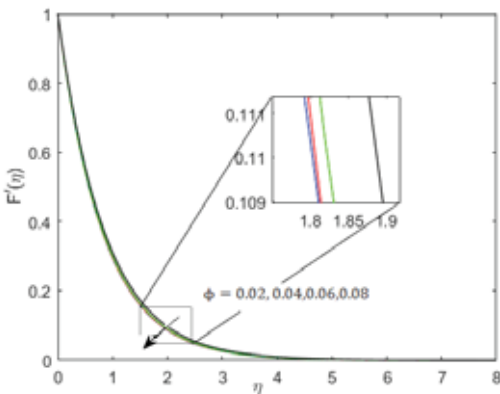


Figure 7. Influence of ϕ on primary velocity $F'(\eta)$

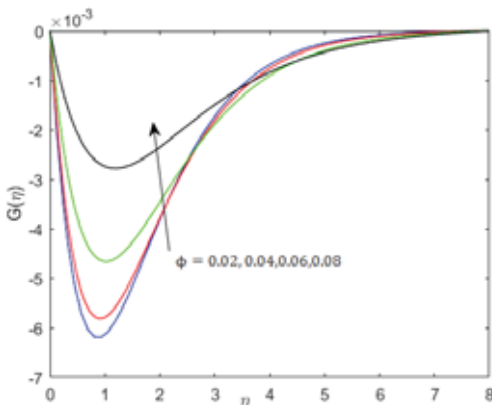


Figure 8. Development of secondary velocity profile with improvement in ϕ

The predominance of the solid Cu – “nanoparticle volume fraction” on flow properties of fluid flow is displayed in Figure 7-Figure 10. From the graphs, it is evident that the addition of the nanoparticle into the base fluid enhances the temperature and decreases the mass diffusivity of the flow. We notice the improvement in the secondary velocity profiles and fall in PVG due to the increase in ϕ .

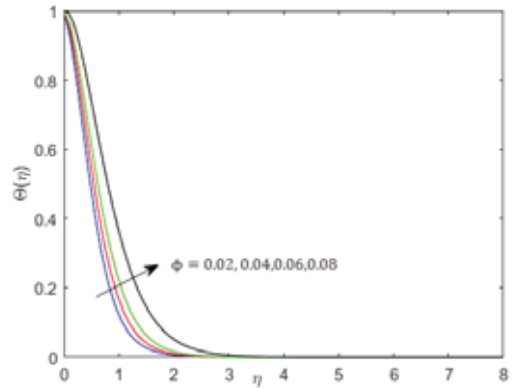


Figure 9. The upshoot of temperature with change in ϕ

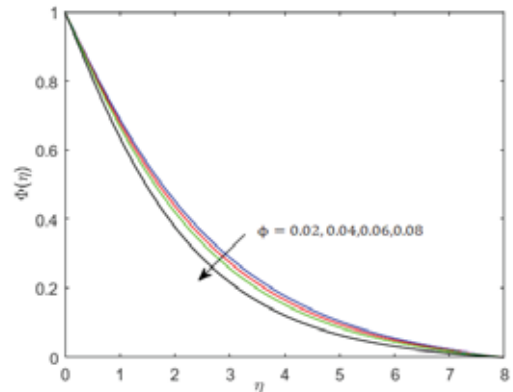


Figure 10. The variation in the concentration profile with ϕ

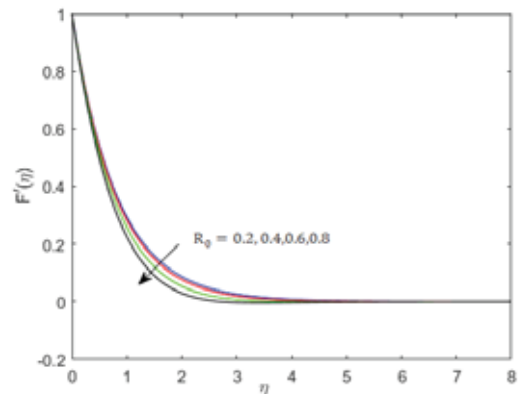


Figure 11. Impact of R_0 on $F'(\eta)$

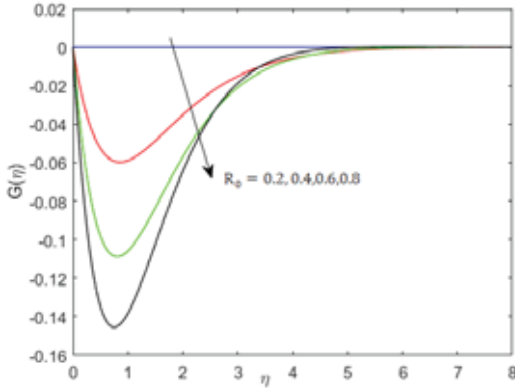


Figure 12. The change in $G(\eta)$ with changes in R_0

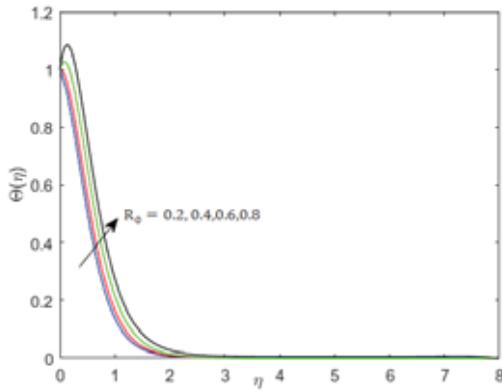


Figure 13. Impact of R_0 on $\theta(\eta)$

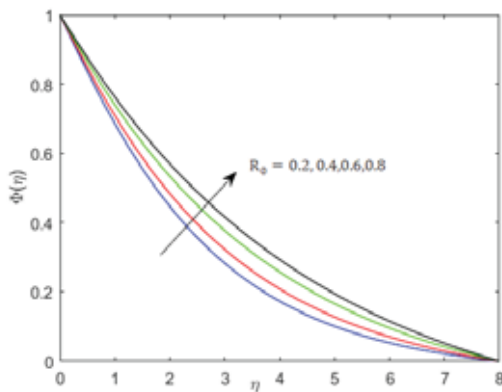


Figure 14. The influence of R_0 on $\Phi(\eta)$

Figure 11-Figure 14 shows the influences of the rotation parameter on the velocity, concentration, and temperature BLs of the NF fluid flow. The statistics display that the increase in the R_0 value improves the concentration and the temperature of the flow but leads to the downfall of the speed of the fluid. Increasing the rotation generally causes the particle motion close to the boundary to slow down. These factors contribute to the rise in temperature and concentration profiles.

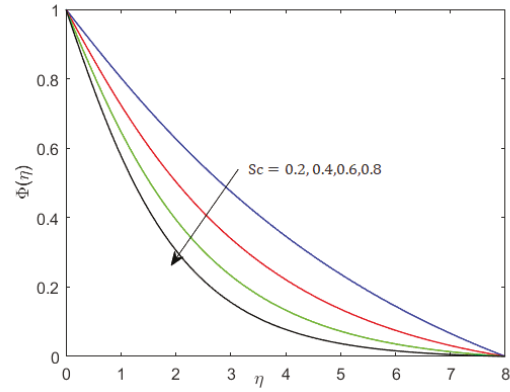


Figure 15. The outcome of Sc 's effect on $\Phi(\eta)$

Schmidt number is the ratio of the shear component for diffusivity viscosity/density to the mass-transfer diffusivity. This equation materially connects the hydrodynamic and the mass-transfer BLs. Thus, from Figure 15 we understand that the rise in Sc diminishes the concentration profile.

TABLE 4. displays the numerical values of the physical quantities of industrial interest for various values of the parameters involved in the modified flow governing equations. From the table, we observe that the improvement in Ec leads to the fall in local Nusselt number due to the reason that the rise Ec results in the fall in thermal BL. The enlargement of the values of k_1 and R_0 lead to the fall local Sherwood number values, whereas we observe the opposite behaviour when the ϕ and Sc values increase as seen from the tabulated value. The primary and secondary skin friction values improve with k_1 and decay for the rise in the values of ϕ and R_0

TABLE IV.
CALCULATED VALUES OF $\frac{1}{(1-\phi)^{2.5}}F''(0)$, $\frac{1}{(1-\phi)^{2.5}}G'(0)$, $-\frac{k_{nf}}{k_f}\theta'(0)$ AND $-\frac{1}{(1-\phi)}\phi'(0)$ FOR DIFFERENT VALUES OF THE
PHYSICAL PARAMETERS SUCH AS Ec, Sc, R_0, ϕ and k_1

R_0	Ec	Sc	ϕ	k_1	$Re_x^{1/2}C_{fx}$	$Re_x^{1/2}C_{fy}$	$Re_x^{-1/2}Nu_x$	$Re_x^{-1/2}Sh_x$
0	0.5	0.5	0.5	0.5	-1.111816	0	0.41709	0.345995
0.2					-1.288031	-0.171253	0.364229	0.334726
0.4					-1.303946	-0.193361	0.290194	0.329548
0.6					-1.34511	-0.370777	0.098932	0.317088
0.8					-1.400148	-0.52773	-0.156678	0.302363
0.2	0.2	0.2	0.02	0.5	-1.288196	-0.019665	1.296906	0.327212
	0.4				-1.288196	-0.019665	0.674597	0.327212
	0.6				-1.288196	-0.019665	0.052309	0.327212
	0.8				-1.288196	-0.019665	-0.570017	0.327212
0.2	0.5	0.5	0.02	0.5	-1.224904	-0.018701	0.402254	0.330155
			0.04		-1.288197	-0.019665	0.36346	0.334671
			0.06		-1.354621	-0.020648	0.32121	0.339555
			0.08		-1.424474	-0.021652	0.275239	0.344818
0.2	0.5	0.5	0.02	0	-1.052069	-0.026512	0.78951	0.366961
				0.5	-1.288197	-0.019665	0.36346	0.334671
				1	-1.662988	-0.014328	-0.343836	0.295102
				1.5	-1.821711	-0.012902	-0.651519	0.281863
0.2	0.5	0.2	0.02	0.5	-1.288197	-0.019665	0.36346	0.201807
		0.4			-1.288197	-0.019665	0.36346	0.289629
		0.6			-1.288197	-0.019665	0.36346	0.379276
		0.8			-1.288197	-0.019665	0.36346	0.465216

VI. CONCLUSIONS

The 3D rotational flow of *Cu + water* NF across an elongating sheet is studied to examine the effects of viscous dissipation and porosity on fluid flow parameters. We utilised the Lobatto IIIa fourth-order approach in MATLAB to evaluate the data. We next analysed the data mathematically and visually. The following are the paper's main takeaways:

- The SVG amplifies with the boost in ϕ , and k_1 whereas the PVG displays the opposite effect.
- With the amplification of the rotation parameter, nanoparticle volume fraction, internal energy and k_1 the temperature of the fluid experiences an improvement
- The local Nusselt number declines with an increase in the Eckert number.
- The surge in the Schmidt number improves the rate of diffusivity and decreases the concentration of the species.

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